

1 **A flow-based platform hyphenated to on-line liquid chromatography for automatic**  
2 **leaching tests of chemical additives from microplastics into seawater**

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4 Kateřina Fikarová<sup>1,2</sup>, David J. Cocovi-Solberg<sup>2</sup>, María Rosende<sup>2</sup>, Burkhard Horstkotte<sup>1</sup>, Hana  
5 Sklenářová<sup>1</sup> and Manuel Miró<sup>2\*</sup>

6 <sup>1</sup>Charles University, Faculty of Pharmacy in Hradec Králové, Akademika Heyrovského 1203, 500 05 Hradec  
7 Králové, Czech Republic

8 <sup>2</sup>FI-TRACE group, Department of Chemistry, University of the Balearic Islands, Carretera de Valldemossa km  
9 7.5, E-07122 Palma, Spain

10  
11 **Abstract**

12 An automatic flow-based system as a front end to liquid chromatography (LC) for on-line dynamic leaching of  
13 microplastic materials (polyethylene of medium density and poly(vinyl chloride)) with incurred phthalates and  
14 bisphenol A is herein presented. The microplastic particles were packed in a metal column holder, through  
15 which seawater was pumped continuously by resorting to advanced flow methodology. Each milliliter of the  
16 leachable (bioaccessible) fraction of chemical additives was preconcentrated on-line using a 10 mm-long  
17 octadecyl monolithic silica column placed in the sampling loop of the injection valve of a HPLC system that  
18 served concomitantly for analyte uptake and removal of the seawater matrix. After loading of the leachate  
19 fraction, the LC valve was switched to the inject position and the analytes were eluted and separated using the  
20 monolithic column (Onyx C18HD 100×4.6 mm) applying an optimized acetonitrile/water gradient and UV  
21 detection at 240 nm. The automatic flow method including dynamic flow-through extraction, on-line sorptive  
22 preconcentration, and matrix clean-up was synchronized with the HPLC separation, which lasted ca. 9 min. The  
23 only two currently available multi-component certified reference materials (CRM) of microplastics (CRM-PE002  
24 and CRM-PVC001) were used for method development and validation. Out of the eight regulated phthalates  
25 contained in the two CRMs, only the 2 most polar species, namely, dimethyl phthalate and diethyl phthalate  
26 as well as bisphenol A, were leached significantly by the seawater in less than 2 h, with bioaccessibility  
27 percentages of 51-100%. The leaching profiles were monitored and modeled with the first-order kinetic  
28 equation so as to determine the rate constants for desorption in a risk assessment scenario. Intermediate  
29 precision values of bioaccessibility data for three batches of CRMs were for the suite of targeted compounds  
30  $\leq 22\%$ .

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\* Corresponding author: E-mail: manuel.miro@uib.es

31 This work for the first time reports a fully automatic flow method with infinite sink capacity (i.e., using a surplus  
32 of extracting solution) for the target species able to mimic the leaching of additives from plastic debris across  
33 the water body in marine settings under the worst-case extraction conditions.

34

35 **Keywords:** microplastics, phthalates, bisphenol A, seawater, dynamic leaching, automation

36

## 37 1 Introduction

38 With growing production of plastics over the past decade exceeding 350 million tons [1], the problem with  
39 plastic litter worldwide grows ever faster. Only a part of the plastic waste is recycled while the rest is stored in  
40 the landfill and it is estimated that up to 10% of plastic production ends up in the ocean [2].

41 In the early 2000s, micrometric particles of plastic debris, called microplastics, have firstly been found in ocean  
42 waters [3]. Throughout recent years, research on microplastics in environmental settings has attracted a great  
43 deal of interest, which is well documented by many reviews published recently [2,4-12] and a rising  
44 environmental problem addressed in media of all kinds [13,14]. The size range of microplastics is not uniformly  
45 defined; however, most sources set the upper limit to 500  $\mu\text{m}$ , beyond that the term mesoplastics is  
46 recommended [4]. Over time, particles degrade to even smaller sizes (so-called nanoplastics, up to a few  $\mu\text{m}$ )  
47 [4]. Microplastics are divided into 2 groups: (i) Manufactured microscale particles and virgin plastic pellets that  
48 are called primary microplastics and used directly in personal care products and cosmetic formulations such  
49 as body scrubs, toothpaste, and deodorants or indirectly (e.g., virgin plastic pellets) as precursors of polymer  
50 consumer products [2,7]. (ii) Those resulting from the biological or chemical breakdown and weathering of  
51 macroplastic debris into small fragments in the beach environment that enter via rivers, wind, or ship litter, or  
52 originating directly from abrasion processes, e.g. car tires [2,4], and are called secondary microplastics.  
53 Leaching or UV-induced breakdown of plasticizers makes the secondary microplastic debris even more brittle  
54 [4,15].

55 Because of the micro-sized dimension of the plastic particles, the probability of ingestion by various types of  
56 marine biota including zooplankton, worms, mussels fish, mammals, and seabirds increases [7]. Beside  
57 chemical toxicity and mechanical damage [2], a current concern occurs about translocation into tissues as one  
58 of the most important toxicity pathways of microplastics in fish and aquatic invertebrates [9]. Notwithstanding  
59 the fact that the role of microplastics as vectors of chemical contaminants adsorbed on the hydrophobic  
60 surfaces or bound to their inner structure by physical interactions is still debated [2,10,16,17], plastic debris  
61 are regarded as potentially having deleterious effects on marine organisms on account of the leaching of plastic  
62 additives, such as plasticizers, antioxidants, colorants, lubricants, flame retardants as well as residual  
63 monomers under environmental conditions [2,18,19]. All of the above organic chemicals can accumulate in  
64 tissues of animals and by this affect the food chain detrimentally. Moreover, plastic additives can be released

65 easily during the generation of secondary microplastics by weathering breakdown of beached plastic debris.  
66 Another problem is that the sedimentation speed of microplastics is low, hindering their elimination in  
67 wastewater treatment plants and allowing them to remain a long time in the upper, biologically active ocean  
68 layer [20].

69 Phthalates are esters of phthalic acid, which possess a wide range of polarity. High molecular mass phthalates,  
70 such as diethylhexyl phthalate (DEHP), diisononylphthalate (DINP), di-n-octyl phthalate (DNOP) and diisodecyl  
71 phthalate (DIDP) are used mainly as plasticizers. On the other hand, low molecular mass phthalates, like  
72 dimethyl phthalate (DMP), diethyl phthalate (DEP) and di-n-butyl phthalate (DnBP) are frequently found as  
73 constituents of cosmetics and adhesives [21-23]. Phthalates are considered endocrine disruptors already at  
74 the low ng/L and µg/L levels [24]. The European Parliament Directive 2005/84/EC prohibit adding DEHP, DnBP,  
75 and benzyl butyl phthalate (BBP) in a concentration higher than 0.1% by mass of the plasticized material to all  
76 toys and childcare articles due to their potential reproductive toxicity. For higher molecular mass phthalates,  
77 namely, DINP, DIDP, and DNOP, the Directive restriction only applies to toys that can be placed in the mouth  
78 by children [25].

79 Bisphenol A (BPA) is another common organic species in polymer manufacturing and is used as antioxidant or  
80 monomer for polycarbonate plastics. Its high solubility in water makes BPA easily leachable to the aquatic  
81 environment or into the food from polymer packaging. BPA is known estrogen agonist and androgen  
82 antagonist with a variable effect on the human reproductive system. Thus, it is currently regarded as an  
83 emerging contaminant [2]. Despite this, regulation EU No 10/2011/EU and Commission Regulation (EU)  
84 2018/213 of 12 February 2018 still allows using BPA in plastic food contact materials, excepting polycarbonate  
85 drinking containers intended for infants and toddlers [26].

86 The above chemical classes of additives are commonly encountered in packaging materials, often made of  
87 polyethylene (PE) and polypropylene (PP), which represent one of the largest material fraction of microplastics  
88 and marine litters [15]. As for polyvinylchloride (PVC), up to 50% of the weight might be composed of  
89 phthalates [27].

90 There is a wealth of literature on sampling protocols for micro and nanoplastic sampling in sediments and  
91 water columns [28-30] and analytical methods for characterization of the polymers by either FTIR, Raman  
92 spectrometry or pyrolysis GC/MS [5,31-34]. Nevertheless, only a limited number of studies concerned leaching  
93 of the plastic additives from the plastic debris into marine settings [27,35,36]. To the best of our knowledge all  
94 of the reported methods for simulating the potential transfer of additives to the marine environment are based  
95 on manual/batchwise protocols encompassing either end-point leaching with seawater using gentle shaking  
96 [37] or kinetic desorption methods but with low temporal resolution [35,36,38,39].

97 We herein report for the first time an automatic flow-based method for investigation of the leachability of  
98 chemical additives (i.e., phthalate esters and BPA) from microplastics under dynamic extraction conditions  
99 mimicking realistic environmental scenarios, namely, the desorption of littoral plastic debris entering the  
100 marine environment for which the liquid (seawater) to solid ratio tends to infinite. In fact, dynamic extraction  
101 using flow setups has been demonstrated to simulate environmentally and physiologically changing conditions  
102 more accurately than its batch counterparts [40-44]. Our flow system hyphenates in-line leaching of  
103 microplastics with seawater as contained in a metal mini-column for ascertaining bioaccessible pools of plastic  
104 additives under worst-case scenarios in marine settings. Not only extraction but sample preparation using on-  
105 line microsolid-phase extraction ( $\mu$ SPE) is automated for matrix clean-up and analyte preconcentration  
106 followed by switching-valve liquid chromatographic separation. Analytical method validation was  
107 accomplished by employing the two only available certified reference materials (CRM) of PE and PVC in the  
108 market containing micro-sized particles in all instances down to 300  $\mu$ m. Those samples can be categorized  
109 correctly as CRM of microplastics with a known content of phthalates and BPA.

110

## 111 2 Materials and methods

### 112 2.1 Reagents and materials

113 HPLC grade methanol, acetonitrile, and 2-propanol were purchased from Fisher Scientific (Madrid, Spain).  
114 Ultrapure water (Millipore, Bedford, USA) with resistivity  $\geq 18$  M $\Omega$ -cm was used throughout. Analytical  
115 standards of BPA, DMP, DEP, BBP, DnBP were purchased from Sigma Aldrich/Merck KGaA (Darmstadt,  
116 Germany) and diluted or dissolved with methanol (MeOH) to a concentration level of 10,000 mg/L. Standard  
117 stock solutions of bis (2-ethylhexyl) phthalate (DEHP), di-n-octyl phthalate (DnOP) and diisodecyl phthalate  
118 (DIDP) at a concentration level of 1000 mg/L in methanol and diisononyl phthalate (DINP) in acetone were  
119 purchased from SPEX CertiPrep (Metuchen, New Jersey, US). A mixed standard stock solution of 1000 mg/L of  
120 methylparaben (MP, Sigma Aldrich) and of 50 mg/L of benzyl benzoate (BB, Sigma Aldrich,) was used as internal  
121 standard (IS)/quality control (QC) after 100-fold dilution.

122 A multianalyte stock solution in MeOH at 1000 mg/L of DMP, BPA, and DEP and 50 mg/L of BBP and DnBP was  
123 prepared for calibration of the on-line system aimed at the determination of the leachable microplastic  
124 additives. The stock solution was stored at 4°C. Working solutions were prepared by appropriate dilution of  
125 the multianalyte stock solution of standards and IS in 25% (v/v) of 2-propanol: water containing 0.025% (v/v)  
126 acetic acid (AcOH). The blank solution contained internal standards and organic solvent at the same  
127 concentration levels than those of the calibration solutions. For the initial optimization of the LC-based  
128 separation method, a mixed working solution was prepared to contain all of the analytes at the 10 mg/L level  
129 in MeOH.

130 Surrogate sea water was prepared by dissolving the following salts in Milli-Q water according to [4045,4446]:  
131 3.0 mg/L NaF, 20 mg/L SrCl<sub>2</sub>·6H<sub>2</sub>O, 30 mg/L H<sub>3</sub>BO<sub>3</sub>, 100 mg/L KBr, 700 mg/L KCl, 1470 mg/L CaCl<sub>2</sub>·2H<sub>2</sub>O, 4,000  
132 mg/L Na<sub>2</sub>SO<sub>4</sub>, 10,780 mg/L MgCl<sub>2</sub>·6H<sub>2</sub>O, 23,500 mg/L NaCl, 20 mg/L Na<sub>2</sub>SiO<sub>3</sub>·9H<sub>2</sub>O, and 200 mg/L NaHCO<sub>3</sub>.

133 Two standard reference materials (CRM) of PE and PVC microplastics (CRM-PE002 and CRM-PVC001, Spex  
134 CertiPrep, Metuchen, New Jersey, USA) were used for analytical method validation. Polyethylene CRM with  
135 average particle size down to 110 μm (see Fig. S1A) contained DIDP and DINP at a concentration level of  
136 30,000 μg/g, and DMP, DEP, DEHP, DnBP, DnOP, and BPA at a concentration level of 3,000 μg/g; and polyvinyl  
137 chloride CRM with average particle size down to 140 μm and density of ca. 1.40 g/mL (see Fig. S1B) contained  
138 DIDP and DINP at a concentration of 30,000 μg/g, and DMP, DEP, DEHP, DnBP and DnOP at a concentration of  
139 3,000 μg/g. PVC and PE microplastics (CRM-PVCBLK and CRM-PEBLK, Spex Certiprep) without incurred analytes  
140 (blank CRM) were used for QC/QA purposes.

141 The CRM microplastics were packed in a stainless-steel holder (50 mm long, 4.6 mm ID) that was incorporated  
142 in the flow setup in upright position. One of the ends of the column, in the direction of the flow, was furnished  
143 with a plug of melamine foam (3 mm width) acting as a stopper of the plastic microparticles on the basis of its  
144 intricate 3D porous structure with pore diameters as small as 40 μm. A metered amount of 50 mg of the PE or  
145 PVC CRM was weighted directly in the metal holder.

146 A C18 monolithic guard column (Chromolith, 10x4.6 mm) from Merck KGaA (Darmstadt, Germany) was  
147 selected as a solid-phase preconcentration column (PrC) for on-line preconcentration of leachable species and  
148 matrix clean-up.

149 A sonifier device (Model S-450A, Branson Ultrasonics Corporation, Danbury, USA, 400 W) equipped with a 3.2  
150 mm titanium microtip (Branson Ultrasonics Corporation) and an ultrasonic bath (JP Selecta, code 3000683,  
151 generator power of 100 W, Abrera, Spain) were employed for quantitative extraction of the most polar species  
152 from CRM-PE and PVC particles, respectively. In the case of probe sonication, the sample was placed in an ice-  
153 water bath to avoid solvent evaporation.

154

## 155 2.2. Flow Setup

156 The flow analyser (MicroSIA, FIALab Inc., Seattle, US) was composed of an automatic bi-directional syringe  
157 pump (SP1, Cattro, Tecan, Sunnyvale, USA) equipped with a 0.5 mL glass syringe (Hamilton, Bonaduz,  
158 Switzerland) and a low-pressure 10-position Cheminert stream selection valve (VICI AG International,  
159 Schenkon, Switzerland) in combination with an auxiliary stand-alone syringe pump (XCalibur, Cattro) furnished  
160 with a 0.5 mL glass syringe (SP2) and filled with surrogate seawater as a carrier as schematically shown in Fig.  
161 1. Syringe pump 1 (SP1), containing water as a carrier, was connected via a 90 cm long polytetrafluoroethylene

162 tubing (so-called holding coil (HC), 1/16" ID) to the central port of the selection valve, which by computer  
163 control allowed the aspiration of the organic diluent (25% (v/v) isopropanol containing 0.025% AcOH),  
164 calibration solutions, and cleaning solutions (water, MeOH) toward the PrC. SP2 was connected to the CRM  
165 filled extraction column (OUT position) for in-line generation of leaching fractions, which entered into the flow  
166 system via a two T-junction connector (see Fig. 1). Alternatively, SP2 served (in Up position) for matrix-matched  
167 calibration using seawater, thus bypassing the microplastic containing extraction column. The outlet of the T-  
168 junctions communicated with via a stainless-steel mixing coil (200  $\mu$ L, 0.8 mm id) with the PrC placed in the  
169 injection loop of an HPLC valve (see below) by stainless steel tubing (0.5 mm ID, 200  $\mu$ L). The overall fluidic  
170 components of the flow-through system were controlled by the user-friendly CocoSoft 4.5 freeware [47].

171 This assembly was modified for the off-line evaluation of the sorptive capacity of the PrC and the potential  
172 breakthrough of analytes in seawater containing organic diluent (viz., a final concentration of 12.5% (v/v)  
173 isopropanol or a mixture of 15% (v/v) MeOH and 5%(v/v) 2-propanol). The PrC (0.5 cm or 1 cm) was placed  
174 directly to the end of the stainless-steel tubing (0.5 mm ID, 200  $\mu$ L). The column was cleaned with 0.5 mL of  
175 MeOH, then with 1 mL of water. Afterwards, the column was loaded with a mixture of 1 mL of seawater on-  
176 line diluted with 1 mL of standard solution at 20 mg/L of DMP, BPA and DEP and 1 mg/L of BBP and DnBP  
177 containing IS (10 mg/L of MP and 0.5 mg/L BB) in tested organic diluent and 0.025%(v/v) of AcOH. Then, the  
178 column was cleaned with 1 mL of water and eluted with 1.5 mL of MeOH. The eluent was collected in a vial  
179 and 10  $\mu$ L were injected into the HPLC.

180

### 181 2.3 HPLC instrumentation and hyphenation with the flow setup

182 An LC-4000 HPLC system (Jasco, Tokyo, Japan), consisting of a quaternary high-pressure pump (PU-4180), an  
183 autosampler (AS-4050) equipped with a high-pressure injection valve (IV), which was connected to the low-  
184 pressure flow setup, and a photodiode array detector (MD-4017), was used for separation of the bioaccessible  
185 pools of chemical additives. A chromatographic monolithic column (Onyx C18HD 100x4.6 mm) preceded by a  
186 monolithic guard-column (Onyx C18HD 5x4.6 mm), both heated at 30°C (Gecko, Jasco), was used for separation  
187 of phthalates and BPA.

188 For off-line studies of leaching, PrC sorptive capacity and optimization of HPLC separation parameters, the  
189 HPLC injection valve was furnished with a loop of 1/32" ID PEEK tubing and programmed to inject 10  $\mu$ L.  
190 Analytes were detected at 200 nm for maximum sensitivity. For on-line dynamic leaching, the injection loop  
191 contained a high-resolution C18 monolithic PrC (Chromolith, 10x4.6 mm) packed in an aluminum holder  
192 (Phenomenex, Torrance, CA, USA) for on-valve trapping of the analytes from the seawater leachate fractions  
193 and matrix removal.

194 Switching-valve elution from PrC and chromatographic separation of analytes (DMP, DEP, BPA, BBP, and DnBP)  
195 were performed in gradient mode using water (A) and acetonitrile (B) for modulating the mobile phase  
196 composition. The HPLC method consisted of the following steps: (i) 0-14 min delay time, during which the  
197 bioaccessible analytes (in seawater) were loaded onto the PrC. During this delay, the HPLC pump was stopped  
198 for preventing wasting the mobile phase. At minute 13 (t=0 for the HPLC run), the flow-rate of the HPLC pump  
199 was smoothly increased up to 1 mL/min and 40 % of B for column equilibration. At minute 14, the linear  
200 gradient started from 40% B to 90% B in 5 min. Afterwards, the gradient returned to 40% B in 1 min and the  
201 PrC and analytical column were re-equilibrated with the initial conditions of the gradient for 3 min.

202 On account of the higher concentrations of target species in the first leachate fractions, the detection  
203 wavelength was set to 240 nm to guarantee signal linearity over a wide concentration range while improving  
204 detection selectivity. Peak area was used as analytical signal throughout. Operational control, chromatogram  
205 and spectra acquisition, and data processing was done by ChromNAV software.

206

#### 207 2.4 Operational protocol for flow-through dynamic leaching and automatic calibration

208 In the course of the delay time of the HPLC method (0-14 min), the flow analyzer was synchronized with on-  
209 line leaching of microplastics and analysis of a given subfraction of the extraction profile for determination of  
210 bioaccessible pools as indicated as follows: i) the two SP were programmed to get initialized, ii) the HC was  
211 cleaned with MeOH to prevent carry-over (from IS), iii) the PrC was rinsed with 0.5 mL of MeOH and 0.5 mL of  
212 Milli-Q water, iv) 1 mL of seawater was brought to the extraction column (SP2 in position Out) at 0.25 mL/min  
213 and the leachate merged on-line with 1 mL of organic diluent containing the two IS in 25% (v/v) isopropanol  
214 and 0.025% AcOH, also at 0.25 mL/min, whereupon the stream was loaded onto the C18-PrC via the mixing  
215 coil, and v) the PrC was cleaned with 1 mL of Milli-Q water to remove the salt content of the leachates, thus  
216 being ready to start the switching-valve HPLC elution method. The organic diluent added on-line to the  
217 seawater extract served to decrease the pH of seawater from ca. 8 to 4.7 prior to the retention of the  
218 bioaccessible target analytes onto the monolithic PrC.

219 The above protocol was repeated a number of times until the leaching profiles reached the baseline (usually  $\leq$   
220 30 fractions) or the increase of extractability in 5 consecutive subfractions for the overall analytes was  $< 10\%$   
221 of the cumulated bioaccessible amounts. The operational program for on-line leaching (using the flow system)  
222 and HPLC separation lasted 23 min per fraction.

223 For on-line calibration purposes, the very same hyphenated flow system than that depicted in Fig. 1 was  
224 utilized. It should be noted that the standard solutions of phthalates and BPA should be prepared in 25% (v/v)  
225 isopropanol for minimization of losses by adsorption onto the glassware (see below). The only methodological  
226 difference was that the IS-contained calibration standards were aspirated from the multiposition selection

227 valve (see Fig. 1) and merged on-line with seawater pumped simultaneously by SP2 through the bypass tubing  
228 (position Up) so as to perform a matrix-matched calibration to offset the effect of seawater onto the PrC  
229 sorptive efficiency.

230

#### 231 2.5. Synchronization of the HPLC separation with the automatic on-line leaching procedure

232 The HPLC system was first initiated, with an injection delay of 14 minutes, that is, the HPLC injection valve  
233 turned to position 'Load' and waited 14 minutes for sample (extract) loading onto the C18-PrC. The flow system  
234 was manually started at the time that the HPLC valve turned to the 'load' position (see Fig. S2). The sample  
235 preparation method lasted almost 13.5 minutes, and, therefore, the HPLC injection delay was well  
236 synchronized with the sample preparation time. Sample preparation finished ca. 30 s before the HPLC delay  
237 ended, and the flow setup was programmed to wait for the valve turning back to the 'inject' position. When  
238 the valve was turned and the HPLC started to run the separation method of the first leachate fraction, the  
239 electrical signal from the HPLC autosampler was captured by Cocosoft and this caused the flow system to enter  
240 a delay matching the LC separation time (i.e., 9 min). In the very same moment that the LC method finished  
241 and passed to the next sample by turning the injection valve to 'load', CocoSoft was programmed to perform  
242 the next extraction and processing of the next leachate fraction. The signal generated by the HPLC and  
243 captured by CocoSoft allowed resynchronizing both fluidic systems in every fraction to offset the operational  
244 time variability of the mechanical components thus enabling a long term unsupervised operation of the  
245 hyphenated setup.

246

#### 247 2.6. Ultrasound-assisted chemical extraction of additives from microplastics

248 Two simple analytical methods were developed for quantitative extraction of the most polar additives from  
249 the CRM materials with the purpose of mass balance validation. To this end, 50 mg of CRM-PVC microparticles  
250 were extracted with 10 mL of ACN by probe ultrasonication for 30 s at 10% power. Afterwards, the suspended  
251 microplastics were filtered (0.45  $\mu\text{m}$ , Nylon syringe filter) and the supernatant was made to 25 mL with ACN.  
252 The second method involved extraction of 50 mg of CRM-PE microparticles with 10 mL of a 1:1 (v/v) mixture  
253 of tetrahydrofuran (THF) and isopropanol assisted by bath ultrasonication for 30 min. Undissolved  
254 microplastics were filtered through 0.45  $\mu\text{m}$  Nylon filters and the extract made to 25 mL with 1:1 (v/v) THF and  
255 isopropanol. The content of DMP, DEP, and BPA, was determined by HPLC-UV (injection of 10  $\mu\text{L}$ ).

256



## 257 3 Results and discussion

### 258 3.1 Configuration of the flow system for on-line dynamic leaching of microplastics and automatic 259 processing of the extracts

260 Preliminary dynamic leaching tests with seawater were performed in a semi-automatic mode by coupling the  
261 microplastic-loaded stainless-steel column containing either PE or PVC (with or without incurred analytes) and  
262 the C18-PrC in series, followed by elution of the retained plasticizers and BPA from the C18 microcolumn by  
263 100% MeOH and off-line HPLC analysis. The miniaturized SP was proven able to endure the pressure drop  
264 caused by the two mini-columns in series. Only five out of nine species from the two CRMs with incurred  
265 analytes were identified as bioaccessible across the seawater leachates, that is, DMP, DEP, BPA, DnBP, and  
266 BBP, which were thus selected as the target compounds of the automatic flow-through leaching method in the  
267 remainder of this work. No detectable concentrations of phthalates and BPA were however found in the  
268 leachates of either blank CRM.

269 The automatic flow system should be devised to concomitantly permit the handling of (i) the CRM  
270 microplastics, (ii) the seawater extracts that are subjected to on-line solid-phase extraction, and (iii) the  
271 calibrants as well. On-line calibration across the flow system is a common practice in flow-through sorptive  
272 microextraction approaches to offset non-exhaustive uptake of targets compounds [48,49]. In our case,  
273 aqueous solutions of phthalates and BPA cannot be used as calibrants because of unwanted sorption of the  
274 species on glassware and inner surfaces of the fluorinated tubing of the flow system, even for the most polar  
275 DMP and DEP species. Thus, the addition of organic modifiers should be considered. However, high content of  
276 water-miscible organic solvent might jeopardize the efficient uptake of the most polar species, viz. DMP, by  
277 the reversed-phase C18-PrC. The composition of the on-line seawater leachates should be also tailored to  
278 contain a given percentage of organic modifier to overcome losses of the bioaccessible plasticizers in the way  
279 toward the PrC. The required solvent was therefore added on-line to the leachates by SP1, after aspiration in  
280 the HC, at the confluence before the PrC (see Fig. 1). At first, the maximum content of organic diluent (MeOH  
281 or 2-propanol) that could be added to the seawater without causing salt precipitation was tested. Indeed,  
282 precipitation was observed with  $\geq 40\%$  (v/v) of MeOH or  $\geq 30\%$  (v/v) of 2-propanol.

283 Peak areas of mixed standards containing DMP, BPA and DEP at the 1 mg/L level and 1% (v/v), 5% (v/v), and  
284 10% (v/v) of MeOH were compared against those of a mixed standard in 100% MeOH. It was found that BPA  
285 and DEP were not stabilized by such low concentrations of MeOH (see Table S1). The experiment was repeated  
286 with (i) 2-propanol (5%, 10%, 15% 20% and 25% (v/v)), (ii) increased contents of MeOH (20% and 30% (v/v))  
287 and (iii) a combination of MeOH and 2-propanol (30% and 10% (v/v), respectively). Mixed standards with 5  
288 phthalates and BPA were used in this experiment. The experimental results (see Table S1) showed that the  
289 combination of 30% (v/v) MeOH and 10% (v/v) 2-propanol, i.e. 15% and 5% after on-line dilution of the

290 leachates; and 25% (v/v) of 2-propanol (12.5% after dilution) afforded appropriate stability of all of the target  
291 species inasmuch as recoveries > 91% for DMP, DEP, DnBP, and BPA were obtained as compared with standards  
292 prepared in 100% MeOH. However, selection of the composition of the organic diluent for standards and  
293 leachates should be done on the basis of the analyte breakthrough studies of the 5 target species using the  
294 on-valve preconcentration system.

295 Two lengths of the preconcentration column (5 mm and 10 mm) and two compositions of the organic diluent  
296 (30% MeOH+10% (v/v) 2-propanol and 25% (v/v) 2-propanol) were compared at the 10 mg/L level of DMP,  
297 BPA, and DEP and 1 mg/L of BBP and DnBP. The standard solution (1 mL) was on-line mixed 1:1 with Milli-Q  
298 water or seawater and loaded onto the preconcentration column. Afterwards, the analytes were eluted with  
299 1 mL of MeOH and off-line injected into HPLC (10  $\mu$ L). For the calculation of the extraction efficiency, the same  
300 standard solution (10 mg/L DMP, BPA and DEP and 1 mg/L BBP and DnBP) in 100% MeOH was directly injected  
301 into the HPLC (10  $\mu$ L). Regardless of the column, analyte breakthrough was detected for the most polar species  
302 (DMP), yet the longer the column and the lower the percentage of the organic modifier the better was the  
303 sorption efficiency for the entire suite of compounds with quantitative recoveries of DEP, BPA, BBP, and DnBP  
304 (see Figures S3 and S4). Even though the recovery of DMP was  $\leq$  40%, the sensitivity was sufficient for analysis  
305 of the on-line leachates from microplastics. Therefore, 25% (v/v) isopropanol and the 10 mm PrC were selected  
306 for further on-line experiments.

307 The effect of the seawater matrix on the sensitivity of the sorptive preconcentration method was ascertained  
308 by comparison of the slopes of the on-line calibration graphs for the five analytes as obtained in MilliQ water  
309 against 1:1 diluted seawater, all containing 12.5% (v/v) isopropanol. The *t*-test to compare slopes of regression  
310 lines (based on  $t_{exp}$  and  $t'_{exp}$ ) [50] revealed statistically significant differences at the 0.05 significance level for  
311 the most polar phthalate species. The feasibility of offsetting matrix effects by two internal standards (10 mg/L  
312 MP and 0.5 mg/L BB) was therefore studied. MP and DMP behaved alike in terms of breakthrough and BB alike  
313 the rest of analytes (see Fig. S3 and Fig. S4) yet the use of a matrix-matched calibration with seawater  
314 throughout the kinetic bioaccessibility assays was proven necessary for reliable measurements. The two IS  
315 were, however, added to the organic diluent ("blank" solution in Fig. 1) that merged on-line with the seawater  
316 leachates for QC of the operation of the hyphenated flow system and detect potential clogging effects of PrC  
317 in the time course of the leaching tests. The flow manifold was finally configured for the seawater contained  
318 in SP2 (see Fig. 1) to serve concomitantly as a leaching reagent of the microplastics and matrix modifier of the  
319 standards for accurate quantification of bioaccessible pools of plasticizers and BPA.

320

321 3.2 Configuration of the hyphenated system for on-line  $\mu$ SPE-HPLC analysis

322 Of the various on-line hyphenation modes of  $\mu$ SPE with HPLC [51], heart-cut approaches using pure methanol  
323 or acetonitrile as eluent of the reversed-phase PrC were discarded because of band broadening effects across  
324 the HPLC column for the most polar species, DMP, for which the sensitivity of the on-line  $\mu$ SPE method is the  
325 lowest. A switching valve mode with the C18-PrC integrated into the loop of the HPLC injection valve was used  
326 instead. Initially, a bespoke system configuration enabling the loading of the preconcentration column in  
327 parallel to the chromatographic separation of the analytes concentrated in the previous run was assembled.  
328 To this end, the HPLC IV was left in 'inject' position for 2 min to elute the analytes by the mobile phase  
329 containing  $\leq 40\%$  ACN. Then, the valve was turned back to 'load' position for further conditioning and loading  
330 of the PrC by the low-pressure flow-based system. While there was a clear advantage of time efficiency of the  
331 procedure, the elution strength of the mobile phase was proven insufficient for the less polar analytes (BBP,  
332 DnBP) resulting in a carry-over effect across consecutive runs. Therefore, the final on-line configuration of the  
333 hyphenated system involved the sequential loading of PrC and the analyte elution and separation by the full  
334 HPLC gradient. The time of analysis per fraction increased from 14 to ca. 23 min. Nevertheless, the quantitative  
335 elution of all 5 target analytes without carry-over effects and the unsupervised control of both flow system  
336 and HPLC by user-friendly software throughout the entire dynamic leaching protocol were accomplished. It  
337 should be noted that the loading and elution steps were programmed in a forward-flow mode because of the  
338 minute dimensions of the PrC that acted as a filter and thus avoided the introduction of potentially interfering  
339 species, e.g., precipitated salts at the head of the PrC, into the analytical column.

340

341 3.3 Leaching study and method validation

342 Two standard CRM (see section 2.1) of polyethylene (PE) and polyvinylchloride (PVC) microparticles were  
343 selected for investigation of the feasibility of the hyphenated flow system for the automatic analysis of the  
344 leachable pools of chemical additives from microplastics, and the recording of the temporal extraction profiles  
345 of target species in seawater. The PVC material differed from PE in terms of composition (BPA is absent) and  
346 stronger agglomeration of the microparticles (see SEM images in Fig S1). The shape of the PVC particles was  
347 irregular, but PE particles were rather spherical. Three leaching profiles consisting of a maximum of 40 leaching  
348 fractions (1.0 mL seawater each) were recorded for each material and the average is shown in Fig. 2. The  
349 bioaccessible fraction of a given analyte was deemed quantitatively released when the extraction profile  
350 reached the baseline or the extracted analyte quantity of five consecutive fractions was less than 10% of the  
351 accumulated quantity from all fractions for such analyte. The analytes with lower  $K_{ow}$ , i.e., DMP, DEP, and BPA  
352 were leached rapidly, with a maximum of 30 fractions for extracting the overall bioaccessible pools from PE  
353 and PVC, which corresponded to a maximum extraction time of 120 min (see Fig. 2). Bioaccessibilities of DMP  
354 and DEP from PE in seawater were  $> 84\%$  as compared with values of  $> 79\%$  in PVC (see Table 1). BPA was

355 however only leached from PE by 50% using the dynamic flow-through method. In contrast, a minute and  
356 virtually steady leaching of the less polar BBP and DnBP (< 8%) was observed throughout. The low solubility in  
357 seawater was the limiting factor for the bioaccessibility of species with  $\log K_{ow}>4.5$ . Multiple chromatograms  
358 illustrating the leaching profiles of PE in seawater (fractions 1-25) are overlaid as a representative example in  
359 Fig. S5.

360 The on-line matrix-matched calibration with standards prepared in 25% (v/v) isopropanol and containing the  
361 two IS was fully automated by nesting the various standard solutions to the multiposition valve (see Fig. 1) and  
362 pumping seawater by SP2 in a 1:1 volume ratio. The dynamic linear range for quantification of bioaccessible  
363 species spanned from 0-10 mg/L for DMP, BPA and DEP and 0-0.5 mg/L for DnBP and BBP with correlation  
364 coefficients ( $R^2$ )> 0.9984, and limits of detection (LOD) and quantification (LOQ) at 240 nm (calculated as 3  
365 times the standard deviation (SD) for LOD and 10 times SD for LOQ of the lowest concentration level of the  
366 calibration range divided by the method sensitivity) of 0.03 and 0.1 mg/L for DMP; 0.3 and 0.9 mg/L for BPA;  
367 0.2 and 0.7 mg/L for DEP; 0.03 and 0.1 mg/L for BBP; and 0.01 and 0.03 mg/L for DnBP. The analytical sensitivity  
368 of the five target analytes (given as L/mg-area) was 286,000; 628,000; 837,000; 817,000 and 874,000 for DMP,  
369 BPA, DEP, BBP, and DnBP, respectively. The relative SD for standard solutions at the lowest concentration levels  
370 of the calibration graph, that is 2.5 mg/L for DMP, BPA and DEP and 0.125 mg/L for BBP and DnBP (n=7) ranged  
371 from 0.8 to 3.6%. The intermediate precision of the overall bioaccessible concentrations of DMP, BPA, and DEP  
372 for PE and DMP and DEP as obtained by the summation of the fractions of the kinetic extraction profiles ranged  
373 from 7 to 22% (RSD).

374 Trueness (lack of bias) of the on-line leaching method followed by automatic  $\mu$ SPE for determination of  
375 bioaccessible pools was ascertained by the use of mass balance validation (see Table 1). To this end, the sum  
376 of the leached quantities of each analyte determined by on-line switching valve-HPLC in each fraction and that  
377 remaining in the microplastic particles (immobile fraction) after the leaching study were compared against the  
378 total amount as indicated by the certified values and that obtained by ultrasound-assisted solid-liquid  
379 extraction. At first, the analytical method for quantitative extraction of DMP, DEP, BPA, DnBP, and BBP from  
380 the primary CRM microplastics and the residual (non-bioaccessible) leftovers was investigated. Solvents  
381 compatible with HPLC were selected for this study to avoid reconstitution of the extracts. Batch extraction of  
382 CRM microplastics with MeOH was tested using vortex mixing and ultrasonic bath-assisted extraction (5 min,  
383 100 W). MeOH appeared to have insufficient elutropic strength for stripping out of DMP, DEP, BPA, DnBP,  
384 and BBP from the microplastic particles. Ultrasonic-probe assisted extraction (30 s, 10% power) using  
385 acetonitrile afforded quantitative recoveries (> 96%) for the three analytes in CRM-PVC (See Table S2) but  
386 recoveries for PE were only about 50%, and no improvement was observed by increasing the time of  
387 sonication. For CRM-PE, ultrasonic-bath assisted extraction with 2-propanol for 20 min afforded quantitative  
388 recoveries for all of the analytes except BPA (ca. 60%). To ameliorate the elution strength, mixtures of 2-

389 propanol: acetone (70:30) and 2-propanol: THF (50:50) were explored instead (Table S2). The 2-propanol: THF  
390 mixture using 30 min sonication was finally selected as the extraction solvent for PE (original CRM and residual  
391 microplastics) with absolute recoveries ranging from 91 to 103%.

392 The *t*-tests of comparison of the sum of the bioaccessible concentrations of DMP, DEP or BPA plus their  
393 respective residual fractions against the total amounts as determined by ultrasound-assisted extraction,  
394 following the F-test, revealed the inexistence of statistically significant differences at the 0.05 level for any of  
395 the tested analytes and CRM because the experimental *t* values were in all instances below the  $t_{crit}=3.18$  (see  
396 Table 1). Hereto, the dynamic leaching method for DMP, DEP, and BPA from PE and PVC microplastics as a  
397 ‘front end’ to on-line  $\mu$ SPE-HPLC was free from multiplicative and additive matrix interferences. As for DnBP  
398 and BB, the low percentages of bioaccessibility from PE and PVC ( $\leq 8\%$ ), which were on a par or even lower  
399 than the RSD values of the total concentrations in CRMs, made the validation of the method by mass balance  
400 impracticable.

401 On-line leaching data from PE and PVC of each analyte (Fig. 2) were fitted to a first-order kinetic model for  
402 evaluation of the extraction rates in seawater. The best fit for all the target species ( $R^2 > 0.82$ , see Table 2) was  
403 obtained with a single exponential decreasing equation:

$$404 \quad Y(t)=A \cdot \exp^{-k \cdot t}$$

405 Wherein the parameter A stands for the maximum dynamic bioaccessibility of species per weight unit of  
406 microplastic ( $\mu\text{g/g}$ ) at the initial time, and  $k$  ( $\text{min}^{-1}$ ) is the apparent rate constant. The lack of fit test (LOF) with  
407  $p > 0.05$  in all instances revealed that the variability of the dynamic leaching data was well accounted for with  
408 the parameters specified by the single first-order equation. The theoretical bioaccessibility compiled in Table  
409 2 was calculated as the integral of the exponential equation within the timeframe of  $t=0$  to  $t=\infty$  min, which  
410 equals to  $A/k$ . According to the kinetic constants (see Table 2), DMP and BPA were leached in seawater twice  
411 as rapid as DEP from PE, and DMP was extracted thrice as rapid as DEP from PVC, which indicate the potential  
412 environmental risks posed by DMP and BPA-laden beached PE and PVC microplastics.

413

#### 414 **4 Conclusion**

415 This article reported the proof-of-concept applicability of a versatile instrumental setup based on  
416 programmable flow for automatic dynamic leaching of plastics additives (viz., DMP, BPA, and DEP) from  
417 primary CRM microplastics in seawater, and on-line matrix clean-up and analyte preconcentration from  
418 leachates as a ‘front-end’ to chromatographic separation using monolithic columns. The low-pressure flow  
419 system was proven suitable for pumping of seawater through microplastics contained in a mini-column that  
420 was connected in series with a short C18-monolith preconcentration column placed in the loop of the high-

421 pressure HPLC injection valve without flow backpressure effects. On-line fully automatic matrix-matched  
422 calibration in seawater to offset the breakthrough of DMP across the monolith preconcentration column was  
423 accomplished by resorting to the software-controlled multiposition valve and two synchronized microsyringe  
424 pumps. This setup also served for on-line merging of the leachates with 25% (v/v) isopropanol in a 1:1 volume  
425 ratio to prevent losses of the extracted species on the tubing surfaces of the flow manifold.

426 Fast evaluation of the content of bioaccessible additives from PE and PVC was demonstrated with monitoring  
427 the extraction profiles at near real-time. Experimental data were fitted to a first-order extraction model for  
428 elucidation of the kinetic parameters, including the extraction times and leaching rates of DMP, BPA, and DEP  
429 in seawater. Further research is underway in our lab to broaden the applicability of this work for the  
430 investigation of the oral bioaccessibility of beached microplastics with incurred organic emerging contaminants  
431 to ascertain the potential role of microplastics as vectors for contaminants in marine settings.

432

#### 433 **Acknowledgments**

434 MM, DJCS and MR acknowledge financial support from the Spanish State Research Agency through projects  
435 CTM2017-84763-C3-3-R (AEI/FEDER, EU) and CTM2017-90890-REDT (AEI/FEDER, EU). KF acknowledges  
436 financial support from the STARSS project (Reg. No. CZ.02.1.01/0.0/0.0/15\_003/0000465) co-funded by ERDF  
437 and the support by the Charles University (Project SVV 260 412). The authors are grateful to Prof.  
438 František Švec for fruitful discussions. Scanning electron micrographs of the PE and PVC microplastics were  
439 kindly taken by Dr. Ferran Hierro from the Scientific and Technical Center (SCT) of the University of the Balearic  
440 Islands.

1 **Table 1: Bioaccessible concentrations in seawater and mass balance validation of the automatic on-line**  
 2 **leaching method for the determination of DMP, BPA and DEP from PE and PCV microplastics\*.**

Sample	Target	Fractions	Bioaccessibility [mg/g]	Residue [mg/g]	Sum [mg/g]	Ultrasound- assisted Extraction [mg/g]	Certified value [mg/g]	$t_{exp}^{**}$
PE	DMP	20	2.3±0.3	0.10±0.03	2.4±0.4	2.71±0.08	2.977±0.178	2.83
	BPA	20	1.7±0.3	1.70±0.07	3.4±0.3	3.04±0.05	3.001±0.180	1.38
	DEP	30	3.0±0.7	0.31±0.06	3.4±0.5	2.88±0.03	2.998±0.180	1.38
PVC	DMP	15	2.4±0.4	0.6±0.2	3.0±0.5	3.03±0.07	3.005±0.180	0.01
	DEP	25	2.6±0.2	0.4±0.1	2.96±0.08	3.04±0.04	3.001±0.180	1.20

3 \* Results are given as the average of three or four replicates ± standard deviation

4 \*\*  $t_{crit} (\alpha=0.05) = 3.18$

5

6

7

1 **Table 2: Kinetic and statistical parameters of the first-order mathematical model for the description of the on-**  
 2 **line leaching method of chemical additives from PE and PVC microplastics**

Sample	Target	Extraction time (min)	R <sup>2</sup>	k (min <sup>-1</sup> )	Theoretical bioaccessible (mg/g)	F value	Fcrit (α=0.05)	LOF test p (>0.05)
PE	DMP	80	0.910	0.064±0.003	1.66 ± 0.08	0.08	1.59	1
PE	BPA	80	0.820	0.056±0.003	1.11 ± 0.07	0.28	1.59	>0.999
PE	DEP	120	0.820	0.026±0.001	2.7 ± 0.2	0.11	1.59	1
PVC	DMP	60	0.973	0.093±0.003	1.91 ± 0.08	0.13	2.06	>0.999
PVC	DEP	100	0.918	0.031±0.002	2.7 ± 0.2	0.38	2.06	>0.995

3  
4



1 **Figure Captions**

2 Figure 1: Schematic illustration of the flow system configuration for in-line leaching of chemical  
3 additives from microplastics as a 'front end' to on-line  $\mu$ SPE and HPLC separation. EC: extraction  
4 column, HC: holding coil, HV: head valve, MC: Mixing coil (40 cm, 0.8 mm id), PrC: C18 monolithic  
5 preconcentration column (10  $\times$  4.6 mm); SV: selection valve; IV: HPLC injection valve.  
6

7 Figure 2: Kinetic extraction profiles (real and fitted to a single first-order equation) of DMP, BPA and  
8 DEP from CRM-PE and CRM-PVC microplastics as obtained from on-line dynamic leaching coupled to  
9 preconcentration and on-line HPLC analysis.  
10

11

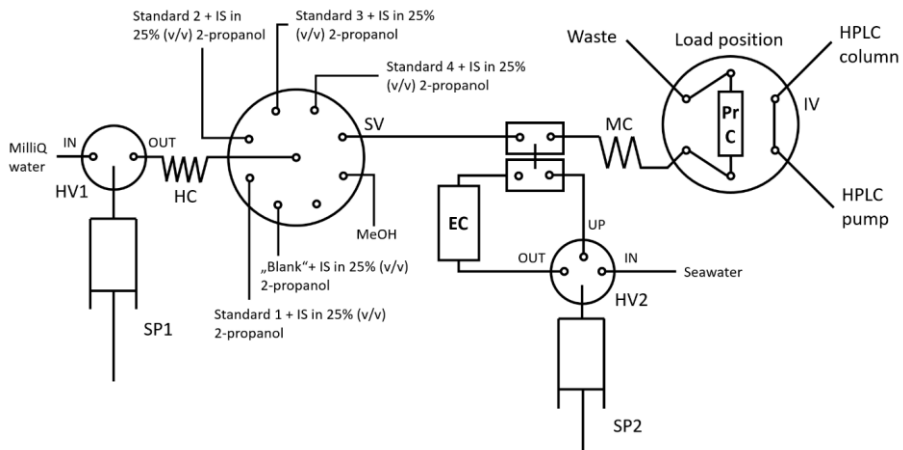
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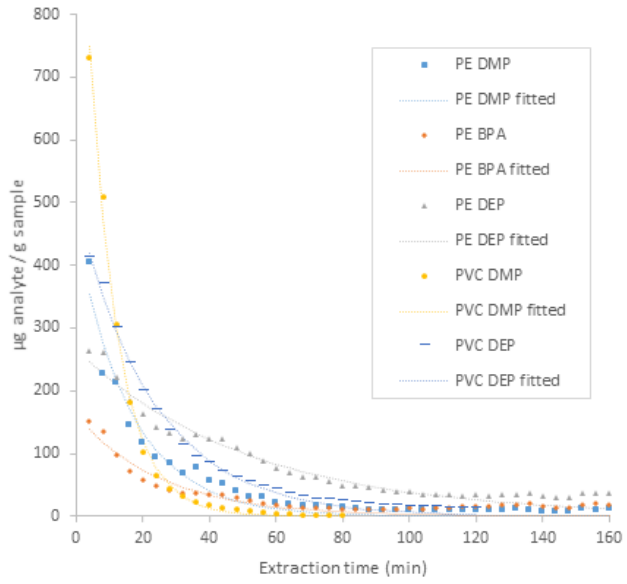
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1 Figure 1



1 **Figure 2**

2



3

4

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